

INDION[®] 2250 H

Hydrochloric acid Regeneration

Description

INDION 2250 H is a controlled particle size premium grade strong acid cation exchange resin containing sulphonic acid groups. It is based on cross-linked polystyrene and has a gel structure. The resin has high capacity and excellent kinetics.

Applications

De-ionising

INDION 2250 H is used in coflow and counter flow modes as a first stage in demineralising for the removal of cations. INDION 2250 H can be used with INDION GS 3000 Cl in mixed bed and condensate polishing units.

Characteristics

Appearance	:	Golden yellow to brown beads
Matrix	:	Styrene divinylbenzene copolymer
Functional Group	:	Sulphonic acid
Ionic form as supplied	:	Hydrogen, H ⁺
Total exchange capacity	:	1.8 meq/ml, minimum
Moisture holding capacity	:	49 -55 %
Shipping weight *	:	780 kg/m ³ approximately
Fines content (<0.42 mm)	:	0.5%, maximum
Uniformity co-efficient	:	1.2, maximum
Effective size	:	0.50 to 0.65 mm
Maximum operating temperature	:	120°C
Operating pH range	:	0 to 14
Volume change	:	Na to H, 8 % approximately
Resistance to reducing agents	:	Good
Resistance to oxidizing agents	:	Generally good, chlorine should be absent

* Weight of resin, as supplied, occupying 1 m³ in a unit after backwashing & draining.

Applications

Two stage de-ionising

Two stage de-ionising uses two units in series - the first containing INDION 2250 H as cation exchanger and second containing strong base anion exchanger Type I resins such as INDION FFIP/GS 300/GS3000/810 or Type II resins such as INDION NIP/GS 400/820.

Mixed bed de-ionsing

When treated water of highest possible quality is required, INDION 2250 H strong acid cation exchange resin is used with INDION FFIP/GS3000 in a mixed bed unit. A mixed bed is often operated as the last unit in a de-ionising stream to act as a "polisher" for producing water of highest quality.

Typical operating data

Two stage/multiple stage de-ionising	Co-Flow Regeneration	Counter Current regeneration
Minimum bed depth	0.75 m	1.0 m
Treatment flowrate	45 m ³ /h m ² , maximum	45 m ³ /h m ² , maximum
Pressure loss	Refer Figure 12	Refer Figure 12
Bed expansion	Refer Figure 11	Refer Figure 11
Backwash.....	9 m ³ /h m ² for 5 minutes	9 m ³ /h m ² till effluent is clear*
Regenerant	Hydrochloric acid (4.0 to 5.0% w/v)	Hydrochloric acid (2.5 to 5.0% w/v)
Regenerant flowrate	3-18 m ³ /h m ²	3-18 m ³ /h m ²
Regenerant injection time	15 minutes, minimum	20 minutes, minimum
Slow rinse	2.5 m ³ /m ³ upto 5/6 injection flowrate	2-3m ³ /m ³ at injection flowrate
Final rinse.....	7.5 m ³ /m ³ at 10 m ³ /h m ³ or at treatment flowrate whichever is higher	For 5 minutes at treatment flowrate

* After a set number of regenerations

Operating exchange capacity

Figures 1, 2, 3 and 4 give operating exchange capacity of INDION 2250 H when used in co-flow regeneration mode. Operating exchange capacity of INDION 2250 H in counter current mode depends on :

- Regeneration level
- Alkaline content of feed water
- Sodium content of feed water
- Active bed-depth

Figures 5, 6, 7 and 8 give operating exchange capacity and correction factor of INDION 2250 H in counter current regeneration mode.

Regeneration

Co-flow regeneration

The concentration of hydrochloric acid used in regeneration is 4-5 % w/v.

Counter current regeneration

The concentration of hydrochloric acid used in regeneration is 2.5 to 5 % w/v. For acid dilution and rinsing, decationised water must be used.

To prevent the disturbance of the resin bed during upward acid injection and uprinse, use of down flow of water is employed. Alternatively, a downward air pressure can also be used for the same purpose. Backwashing of complete bed, during every regeneration is not desirable and only subsurface wash must be employed.

Whenever the counter current unit is backwashed, higher than the normal quantity of regeneration has to be used in subsequent injection operation.

Thoroughfare regeneration

When the alkaline hardness is high, use of INDION 236 weak acid cation exchanger preceding INDION 2250 H is recommended.

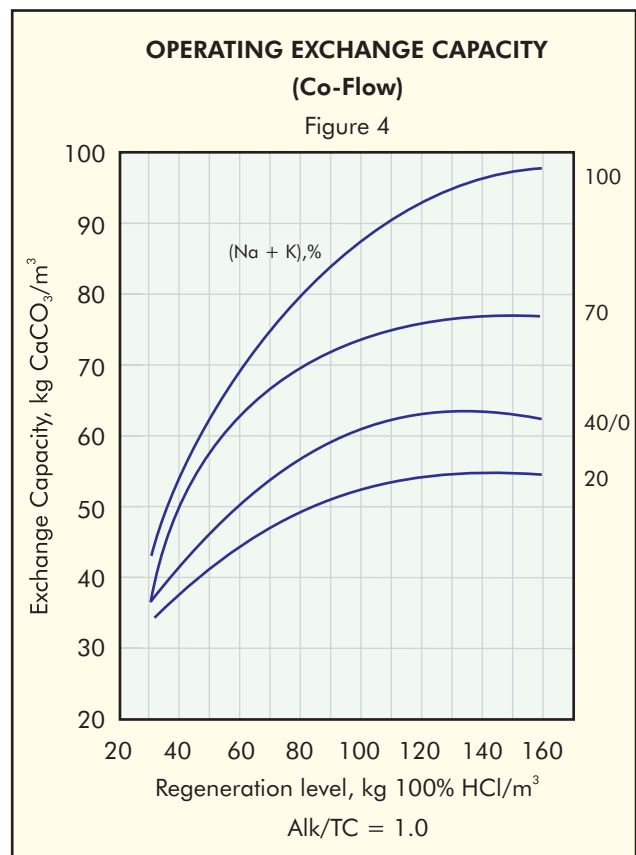
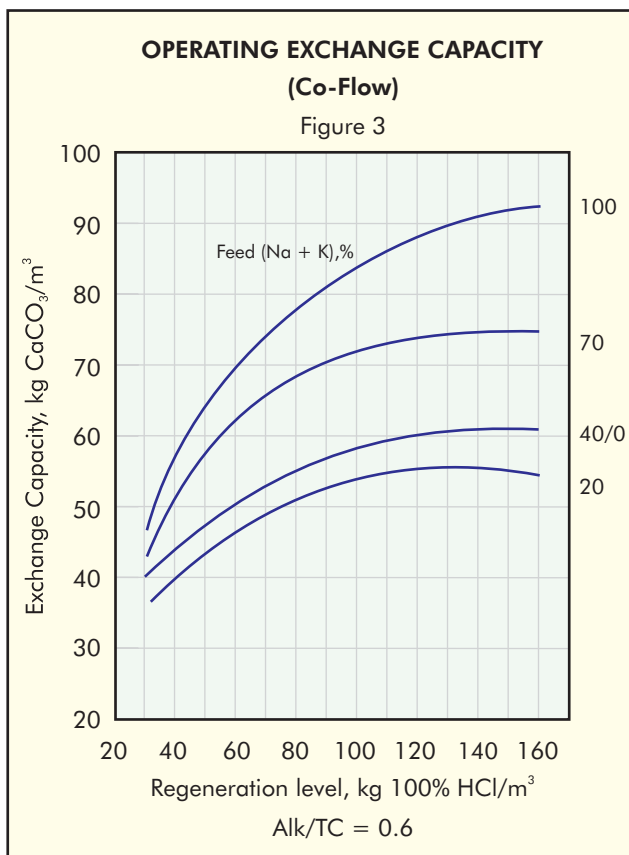
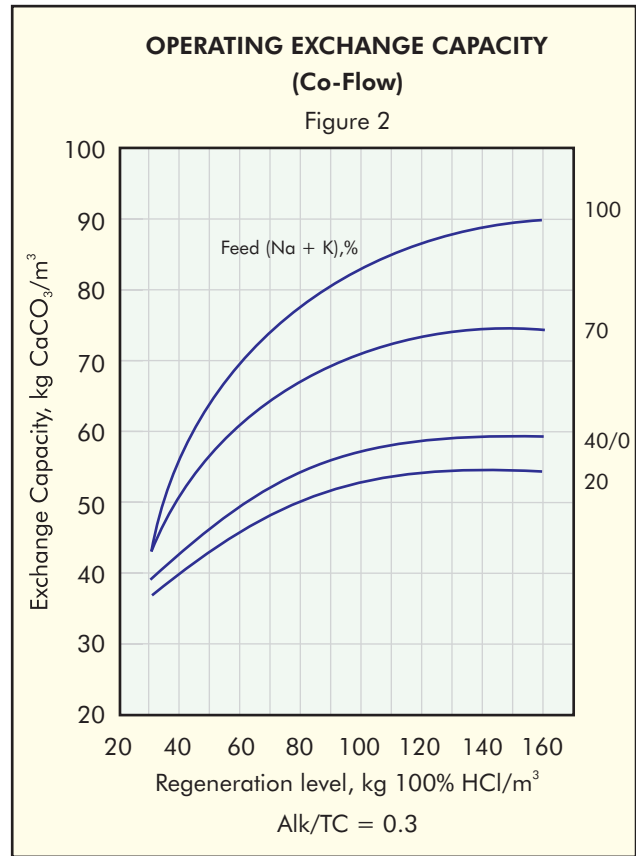
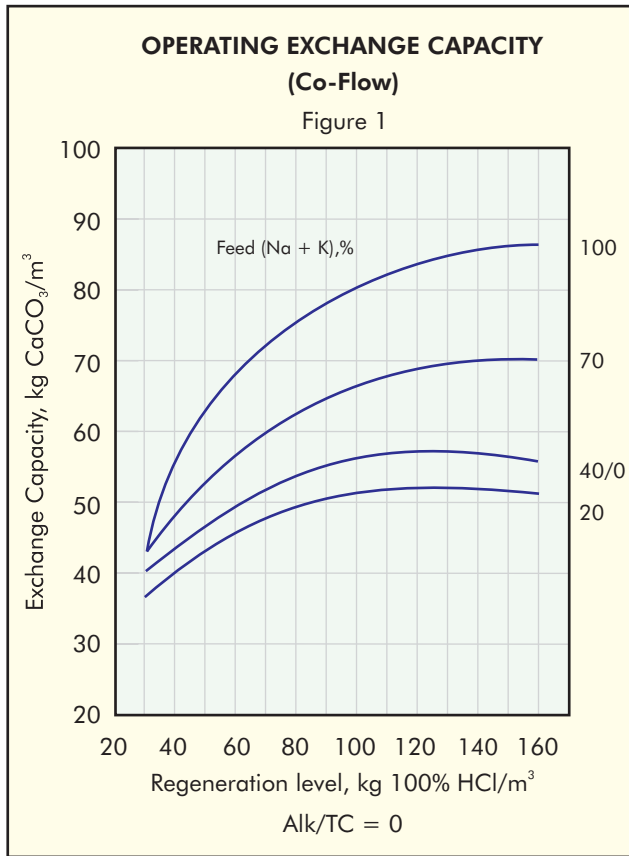
In such cases, the regeneration can be conducted first through strong acid cation exchanger, followed by weak acid cation exchanger. The waste acid from the strong acid cation exchanger is utilised to regenerate the weak acid cation exchanger. This process improves the utilisation of acid and minimises the effluent while obtaining highest quality treated water. This process is commonly referred to as "thoroughfare regeneration".

Treated water quality

Leakage of sodium ions in treated water from strongly acidic cation exchanger depends on:

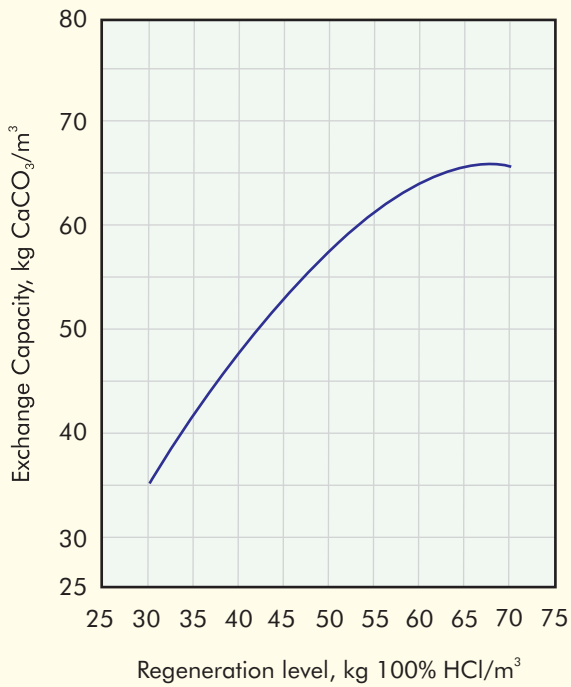
- Sodium content of feed
- Regeneration level employed

Refer to Figure 10 for leakage characteristics of INDION 2250 H in co-flow regeneration mode. The exchange capacities of INDION 2250 H in counter current mode of regeneration are shown in Figure 5. These are based on end point of one ppm of sodium slip expressed as CaCO_3 . For sodium slip less than one ppm, consult us.



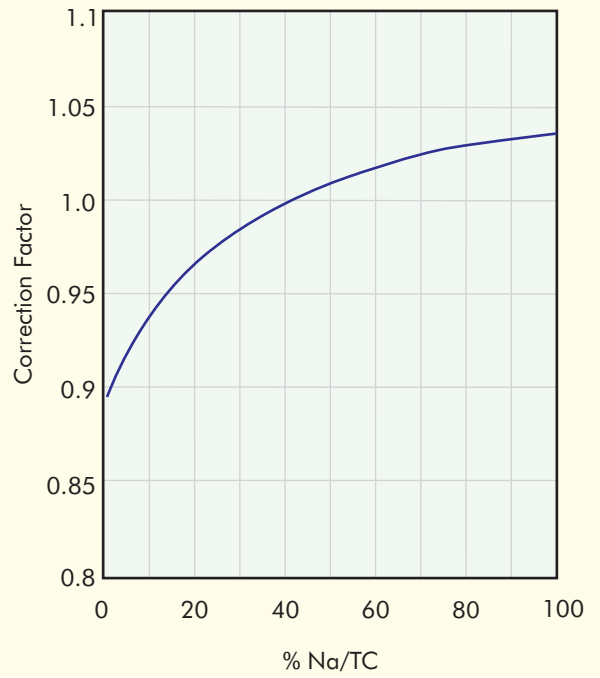
OPERATING EXCHANGE CAPACITY (CCR)

Figure 5



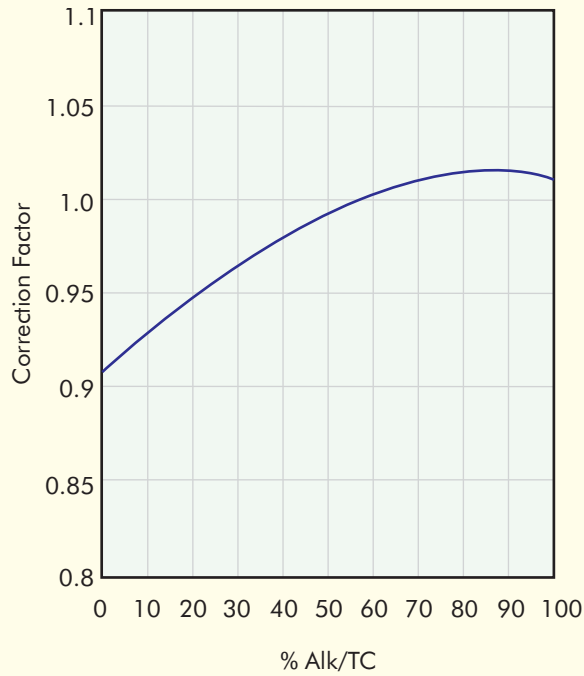
CORRECTION FACTOR FOR FEED SODIUM (CCR)

Figure 6



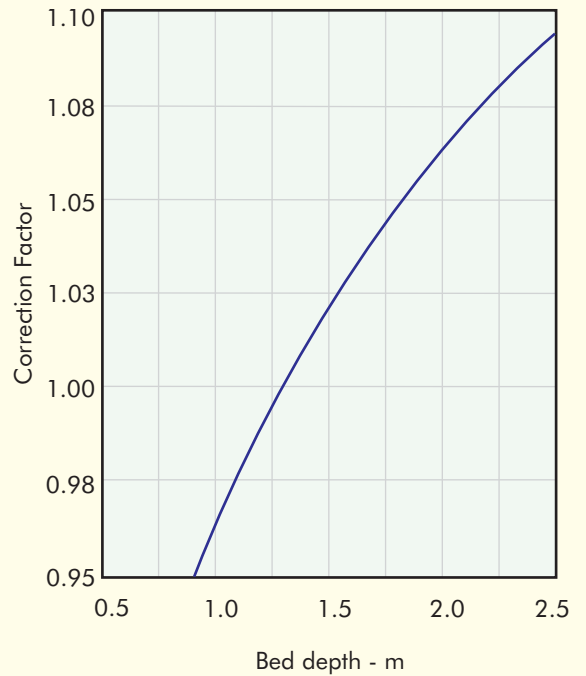
ALKALINE FACTOR FOR FEED ALKALINITY (CCR)

Figure 7



CORRECTION FACTOR FOR BED DEPTH (CCR)

Figure 8



Mixed bed de-ionsing

When used as the cation exchanger in a mixed bed unit, variation with feed water composition in operating exchange capacity is less than that, in two stage deionising. For practical purposes, feed water may be classified as

- Ion exchange softened or demineralised
- Low ionic load influent.

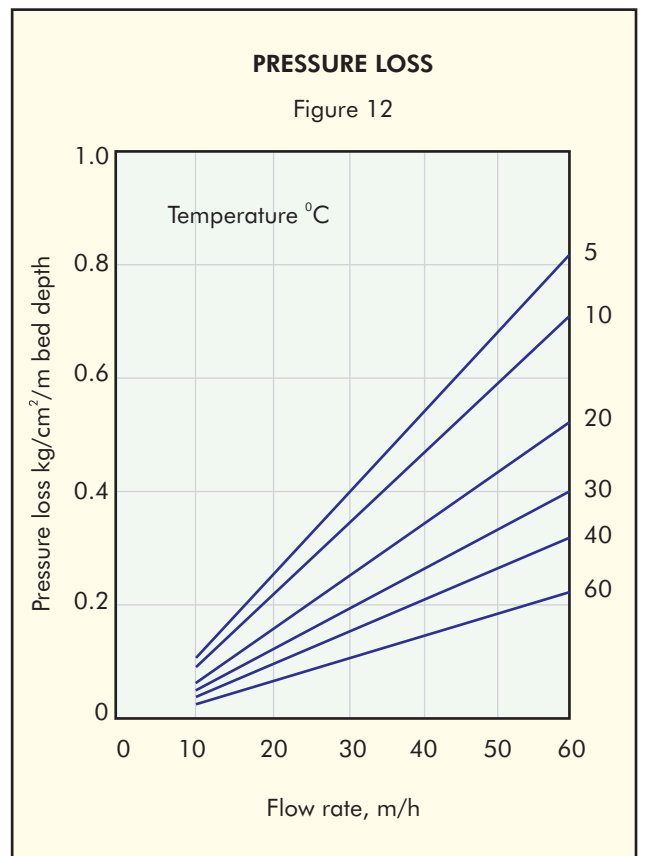
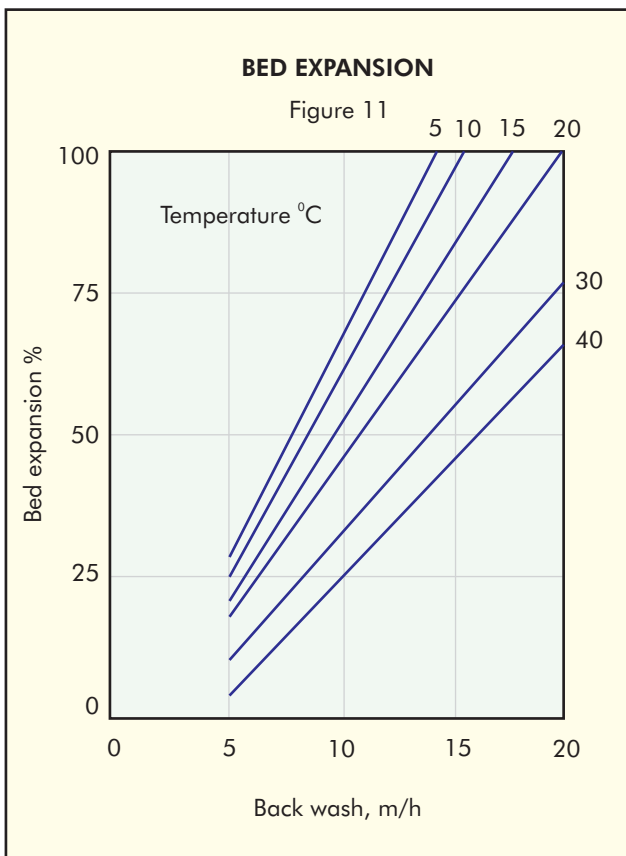
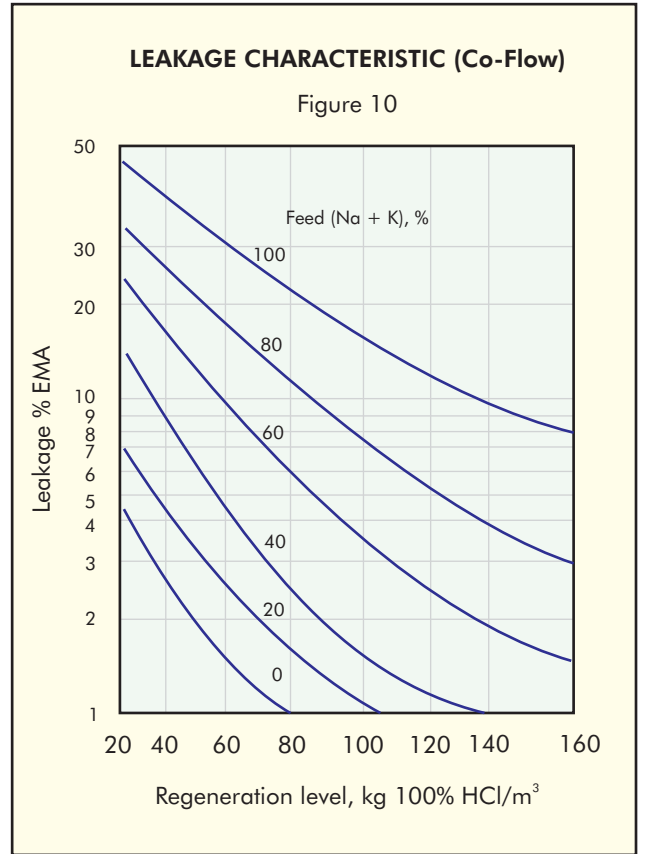
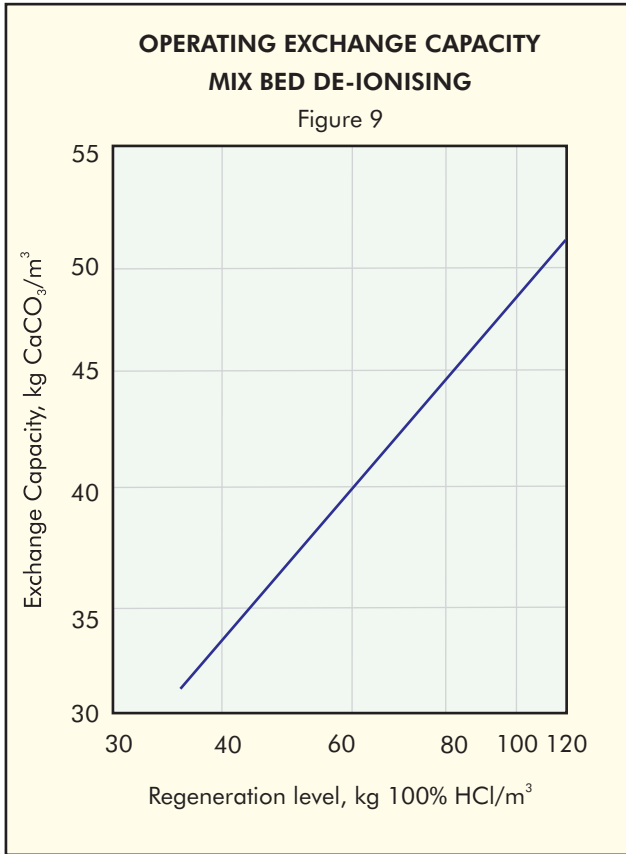
In both cases, INDION 2250 H may be regenerated with hydrochloric acid of 5% concentration.

Figure 9 gives operating exchange capacity when used in a mixed bed unit.

Typical operating data

Mixed bed de-ionising

Total Bed depth	1.0 - 2.4 m using INDION 2250 H and INDION FFIP
Rising space	75% of bed depth
Treatment flowrate	60 m ³ /h m ² , maximum
Pressure loss.....	1.2 kg/cm ² , maximum when using INDION 2250 H & INDION FFIP
Bed separation	9 m ³ /h m ² for 10 minutes
Bed settlement	Allow 5 minutes for separation before commencing injection of regenerants
Acid injection rate	3-18 m ³ /h m ² for 6-10 minutes with 3-5% w/v concentration
Downflow	1.5 m ³ /h m ²
Acid rinse	2 m ³ /m ³ in 10-15 minutes
Unit drain down	Before remixing the resins, the water level should be lowered to approx. 0.4 m above the bed
Bed re-mixed	2 m ³ /minute m ² oil free air at 0.4 kg/cm ² pressure for 10 minutes
Settle bed, refill unit, final rinse	These operations should be carried out in such a way to avoid separation of the two resins. Final rinse to satisfactory water quality should be effected at the treatment flowrate, or at 24 m ³ /h m ² , whichever is greater. Total time required is normally about 5-10 minutes depending upon end point conductivity required.



Use of good quality regenerants

All ion exchange resins are subject to fouling and blockage of active groups by precipitated iron. Hence the iron content in the feed water should be low and the regenerant must be essentially free from iron and heavy metals. All resins are prone to oxidative attack, resulting in problems such as loss of physical strength. Therefore, the regenerant should have as low chlorine content as possible. Good quality regenerant of technically or chemically pure grade should be used to obtain best results.

Packing

HDPE lined bags	25/50 lts	LDPE bags	1 cft/25 lts
Super sack	1000 lts	Super sack	35 cft
MS drums		Fiber drums	
with liner bags	180 lts	with liner bags	7 cft

INDION range of Ion Exchange resins are produced in a state-of-the-art ISO 9001 and ISO 14001 certified manufacturing facilities at Ankleshwar, in the state of Gujarat in India.

To the best of our knowledge the information contained in this publication is accurate. Ion Exchange (India) Ltd. maintains a policy of continuous development and reserves the right to amend the information given herein without notice.

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